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## Horizontal Planar Angular Light Scattering (HPALS) characterization of soot produced in a Laminar Axisymmetric Coflow Ethylene Diffusion Flame

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#### Abstract

In-flame optical characterization of soot is of vital importance to understand soot formation mechanisms as well as to develop and validate accurate soot models. The present work introduces an unconventional methodology adapted to laminar axisymmetric flames that avoids the issue of variable measurement volume with varying scattering angle in the existing light scattering techniques and thus enables the determination of aggregate size with a higher spatial resolution. Coupled with multi-wavelength line-of-sight attenuation measurements, the proposed Horizontal Planar Angular Light Scattering at 532 nm was found able to provide radial profiles of aggregate size, number and diameter of primary spheres, soot volume fraction, and number density in a laminar axisymmetric coflow ethylene/air diffusion flame established over a Gülder burner. The spatial variation of soot optical properties associated with soot maturity was considered in data analysis.

*Keywords:* Planar angular light scattering, Axisymmetric flames, soot maturity, Line-of-sight attenuation, RDGFA

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#### 1 1. Introduction

Soot formation and oxidation mechanisms are still not completely under-2 stood and very challenging to model. Yet, it is becoming imperative to design 3 energy systems that are cleaner and have less impacts on human health and 4 on the environment. To this end, numerical simulation plays a vital role to 5 speed up the design and optimization processes. To gain improved fundamen-6 tal understanding of soot formation mechanisms and to validate soot models, 7 it is essential to obtain complete and robust databases of soot properties in 8 well-controlled and highly stable laminar target flames. Such efforts have 9 been continuously made in the last four decades through developing sophis-10 ticated *in-situ* optical techniques. Among these techniques, Laser Induced 11 Incandescence (LII) has received widespread attention [1]. 12

LII enables the determination of soot volume fraction in complex, transient environments [2] or in very low sooting flames [3]. The LII signal temporal decay rate can be interpreted in terms of soot primary sphere diameters [4, 5].

By conducting LII measurements using two different laser wavelengths, 17 it is possible to determine the ratio of soot absorption functions at the two 18 laser wavelengths, which in turn can be linked to the soot maturity [6-8]. The 19 line-of-sight attenuation (LOSA) and spectral soot emission (SSE) methods 20 are also often used in laminar axisymmetric flames to determine the soot 21 volume fraction and flame temperature [9]. A recent study has shown that 22 LOSA measurements at different wavelengths in the visible and near infrared 23 can provide instructive information on the soot maturation process with a 24 high spatial resolution [10]. Measurement of the volume fraction of incipient 25 soot is extremely challenging due to the very low volume fraction associ-26 ated with the very small incipient soot particles and their weak absorption 27 in the visible. Although the soot aggregate size is important to validate 28 the aggregation and oxidation mechanisms modeled by Population Balance 29 Equation [11, 12] or discrete element methods [13, 14], the above optical 30 techniques are not able to provide information of soot aggregate size, mor-31 phology, and aggregate number density, which are also important quantities 32 to fully characterize soot. To complement the measurements of LII, LOSA, 33 or SSE, the soot aggregate size information has often been obtained through 34 an *ex-situ* method through soot sampling in the flame [15, 16]. However, 35 sampling of nanoparticles is intrusive in nature and can alter the structure 36 of the flame [17, 18]. Moreover, the particle aggregation process can occur 37

in the sampling line as well as smaller particles can be lost by deposition [3]. 38 Finally, the aerosol sizing instruments provide the particle size distributions 39 in either mobility or aerodynamic diameter that have to be interpreted to 40 obtain aggregate size, such as gyration radius, since soot particles are not 41 spherical [12]. These considerations suggest that it is necessary to develop 42 in-situ techniques to measure soot aggregate size. It has been demonstrated 43 some 40 years ago by Santoro et al. [19] that scattering based techniques 44 are able to provide instructive information on soot size. Köylü and Faeth 45 [20] have shown that the interpretation of scattering measurements of soot 46 particles should be performed by a dedicated theory of light interaction with 47 fractal aggregates called RDGFA [21], but not by Mie theory. 48

The reader is invited to refer to Sorensen [22] for more details about that 49 the RDGFA theory. This approach has been extensively used to interpret 50 light scattering measurements of sooting flames [23–25]. Wang and Sorensen 51 [26] have shown the reliability of the RDGFA theory for TiO2 and SiO2 ag-52 gregates and later Chakrabarty et al. [27] for carbonaceous chain aggregates. 53 It has also been shown in some studies that there is good agreement between 54 the size of both aggregates and primary spheres obtained by light scatter-55 ing compared to Transmission Electron Microscopy image analysis [28–30]. 56 However, light scattering techniques have been less favored in recent years 57 compared to LII. Indeed, the current angular light scattering method remains 58 challenging in the sense that the change of scattering angle is accompanied 59 by a change in the measurement volume and thus suffers the problem of a 60 significantly reduced spatial resolution for small and large scattering angles, 61 leading to large uncertainties in the inferred soot aggregate sizes in diffusion 62 flames where physical and chemical quantities display high spatial gradients. 63 Nevertheless, the light scattering techniques are still being improved. An 64 integrated system enabling the measurement of soot size distribution with 65 high temporal resolution has been developed by Oltmann et al. [31]. Bouvier 66 et al. [32] and Zhang et al. [33] have shown the potential of exploiting the 67 spectral dependency of the scattered light. The vertical planar configura-68 tion in an ethylene diffusion flame [34, 35] and in premixed 1D flat flame 69 (McKenna-type burner) [36] has been developed in order to provide a planar 70 description of the soot size. Finally, the light scattering based techniques 71 have been applied in more and more challenging configurations [37, 38] and 72

<sup>73</sup> some efforts have been made to improve the light scattering theories [39, 40]
<sup>74</sup> and the inversion algorithms to accurately recover aggregate size distribution
<sup>75</sup> [27, 41, 42]. These studies illustrate the potential of light scattering tech-

<sup>76</sup> niques and coupled techniques based on light scattering and other optical
<sup>77</sup> diagnostics [43, 44].

Up to now, 2D Multi Angle Light Scattering is the technique providing 78 the aggregate size with the finest spatial resolution [36]. However, the data 79 processing is not simple. Indeed, as explained by Ma and Long [34], the 80 observed image of the laser light sheet interaction with the flame "became 81 narrower in shape and the signal on each pixel was increased due to an 82 increased sample volume". In other terms, the image resolution and the 83 volume of measurement change with the scattering angle when rotating the 84 camera around the burner. Then, an intensity calibration and a correction 85 of distortion of the images are required [34, 36]. These corrections may have 86 an impact on the spatial resolution of such planar light scattering technique. 87 The present work intents to overcome the issue of scattering angle depen-88 dent measurement volume and to improve the spatial resolution of laser-based 89 light scattering technique. This is achieved by the use of an unconventional 90 horizontal laser sheet configuration and the application of this technique is 91 demonstrated in a laminar axisymmetric diffusion flame. This technique 92 enables the determination of soot aggregate size distribution with a high 93 spatial resolution along the radial direction. The coupling of this technique 94 with multi-wavelength LOSA enables the determination of additional infor-95 mation, such as volume fraction, number density, and primary particle size. 96 The combined technique also permits to analyze the data by taking into 97

<sup>98</sup> account the maturity dependence of soot optical properties.

#### <sup>99</sup> 2. Experimental setup, theoretical method, and data analysis

#### 100 2.1. Experimental setup

Figure 1 shows the experimental setup used in this study. The Gülder 101 laminar coflow diffusion flame burner can be accurately moved vertically by 102 means of an Electromechanical cylinder EMC Rexroth. This linear stage 103 facilitates the scanning of scattering measurements at different height above 104 the burner (HAB) with a precision  $< 10 \ \mu m$ . The laminar coflow diffusion 105 flame is generated by delivering pure ethylene through the central fuel tube 106 of the burner at a flowrate of  $0.194 l_{\rm n}/{\rm min}$ . The inner and outer diameters of 107 the central fuel tube are 10.9 mm and 12.7 mm, respectively. The oxidizer is 108 ambient air introduced through the co-annular region of the burner between 109 the central fuel tube and the 90 mm inner diameter of the oxidizer port at 110

<sup>111</sup> 150  $l_n/min$ . These conditions result in a stable laminar diffusion flame with <sup>112</sup> a visible flame height of 75 mm.

Unlike conventional light scattering techniques that utilize a laser beam 113 or a laser sheet orthogonal to the camera axis, the present setup employs 114 a horizontal laser sheet that is wider than the largest flame diameter. This 115 original arrangement can overcome the issue of scattering angle dependent 116 measurement volume at the expense of conducting Abel inversion as shown 117 below. To apply the horizontal planar angular light scattering (HPALS) 118 technique proposed in this study, a Quantel Brillant Easy laser pumped at 119 1064 nm and frequency-doubled at 532 nm is employed. The laser is set for a 120 maximum energy peak per pulse of 185 mJ at 10 Hz with a pulse duration of 121 4 ns (FWHM). The laser output energy is modulated by an internal polarized 122 based attenuator. It is first spatially filtered by using a pin-hole (2.44 mm 123 diameter) in order to preserve the uniform region of the laser beam. Two 124 532 nm dichroic mirrors M1 (CVI Y2-1025-45-A) and M2 (CVI Y2-2037-125 45) are employed to modify the direction of the laser beam and laser sheet, 126 respectively. A variable dielectric attenuator VA1 (Laseroptik L-01543) is 127 used to redirect a part of the laser beam toward a power meter (Coherent 128 PowerMax Model PM10) in order to measure the energy of laser beam during 129 each measurement. 130

The horizontal laser sheet is formed by the combination of three cylindri-131 cal lenses, a plano-concave L1 (f=-40 mm, CVI SCC-20.0-20.3-C), a plano-132 convex L2 (f=300 mm, Thorlabs LJ1996L1), and a second plano-convex L3 133 (f=500 mm, Thorlabs LJ1144L2). This horizontal laser sheet is then pro-134 jected across the flame with a width of 15 mm (larger than the maximum 135 flame diameter  $\sim 10$  mm). A reasonably uniform thickness is obtained with 136 141  $\mu m$  (corresponding to  $2\sigma$ ) measured with a Precision Beam Profiler (Pho-137 ton Inc. Model 2323 USB 2.0 Camera). Note that the polarization state is 138 orthogonal to the laser sheet, i.e., in the vertical direction in Fig.1. 139

The detection system is mounted on a motorized rotating arm (Danaher 140 motion N33HRLG-LEK-M2-00) to enable the signal collection at different 141 scattering angles designated by  $\theta$  (see Fig. 1). The optical collection is com-142 posed of a vertical polarizer P1 (Linear Pola 49 mm, second white arrow 143 in Fig.1) and a long distance microscope system (Infinity CF2+basic unit) 144 mounted with an 1.5 cm extension ring on an ICCD camera (PI-MAX-4, 145 model PM4). The internal laser PTU is employed to trigger the camera to 146 capture the scattering signal for each laser pulse. In order to limit the col-147 lection of the flame natural emission, the ICCD exposure time is reduced to 148

149 14.88 ns.



Figure 1: Experimental setup: The horizontal laser sheet is arranged to cross the flame. The Height Above the Burner can be modified (red arrow) as well as the scattering angle  $(\theta)$  by rotating the camera around the flame axis. M1 and M2 are two dichroic mirrors, L1, L2 and L3 are respectively a cylindrical, plano-concace, and plano convex lenses. VA1 is a variable dielectric attenuator and P1 is a polarizer.

#### 150 2.2. Raw data treatment

Up to 2000 images of  $1024 \times 1024$  pix<sup>2</sup> are accumulated or averaged 151 per condition depending on the signal intensity. The image resolution is 152  $\sim 51 \text{ pix/mm}$ , and the field of an image can cover the width of the flame as 153 depicted in Fig. 2-A. Also, in this figure the region of interest (ROI) is high-154 lighted by the white rectangle of dashed-line. This ROI corresponds to the 155 image of scattering signal of the horizontal laser sheet captured by the ICCD 156 at HAB = 30 mm and a scattering angle of  $14.9^{\circ}$ . The same ROI is also 157 employed with the laser off in order to obtain the background. The profiles 158 after subtracting the aforementioned background are divided by the corre-159 sponding laser energy, the number of accumulations, and the camera gain. 160 The laser sheet uniformity was checked and it was found quite good. The 161 lateral bumps observed in Fig. 2-A are likely caused by multiple scattering in 162 the dense regions (high soot concentration) of the flame. This phenomenon, 163 which is not considered in the present analysis, will be investigated in our fu-164 ture research. Nevertheless, its contribution is considered very small (please 165

note that the scattering intensity is displayed in log scale). Fig. 2-B presents 166 two normalized profiles of two different scattering angles at a given HAB. 167 To avoid a noisy deconvolution, the Python "Savgov filter" (polynomial of 168 order 2 and 31 elements in the averaging window and mirror boundary) is 169 used. The PyAbel's "Hansenlaw" method [45] is used to deconvolute the 170 experimental profiles (Abel inversion, see the dash curves in Fig. 2-B). The 171 obtained radial profile is re-convoluted and compared to the acquired sig-172 nal to check the validity of the deconvolution process (the continuous curves 173 in Fig. 2-B). The re-convoluted scattering signal profiles are in very good 174 agreement with the measurements. 175



Figure 2: A typical light scattering image (left plot) and profiles captured at HAB = 30 mm and at two angles,  $14.9^{\circ}$  (or  $q = 0.0030 \text{ nm}^{-1}$ ) and  $80.2^{\circ}$  (or  $q = 0.0152 \text{ nm}^{-1}$ ) (right plot): (A) Raw scattering signal field and ROI employed (at a scattering angle of  $14.9^{\circ}$ ) and (B) Measured scattering signal profile (symbols), deconvoluted profile (Abel inversion in dash curves), and re-convoluted profiles using the deconvoluted signal (continuous).

#### <sup>176</sup> 3. Light scattering theoretical background

#### 177 3.1. Determination of the absolute scattering coefficient

As illustrated in Fig. 3, the radiative power of scattered light reaching the detector by molecules or particles from an elementary volume dV located at position M and exposed to a planar incident light source with power density  $I_{0}$  (in  $W/m^{2}$ ) can be expressed as,

$$dP_{vv} = I_0 \frac{dK_{vv}}{d\Omega} \Omega dV, \tag{1}$$

where  $\frac{\overline{dK_{vv}}}{d\Omega}$  is the population averaged differential scattering coefficient for 182 vertical-vertical polarization and  $\Omega$  the solid angle related to the detection 183 aperture. The elementary volume can be expressed as dV = dxdydz, where x 184 and y are respectively the positions along the detector and orthogonal to the 185 detector (see Fig. 3) and z is the position along the flame height. The term 186 dS = dxdz corresponds to the elementary surface of the pixel of the ICCD 187 camera which collects the scattered light originated from dV at the scattering 188 angle  $\theta$ . This elementary volume can also be expressed as  $dV = \frac{rdrdS}{\sqrt{r^2 - x^2}}$  with 189 r being the distance of M from the flame center line. 190



Figure 3: Schematic of the HPALS principle (top view).

<sup>191</sup> By assuming negligible laser energy attenuation and self absorption of <sup>192</sup> the scattered signal, the collected signal at position x on the detector can be <sup>193</sup> expressed as an Abel transform of the averaged scattering coefficient, namely <sup>194</sup> the integrated scattering signal along the cord corresponding to position x:

$$P_{vv} = I_0 \Omega dS \times \underbrace{2 \int_x^\infty \overline{\frac{dK_{vv}}{d\Omega}} \frac{r}{\sqrt{r^2 - x^2}} dr.}_{Abel \ transform \ of \ \frac{\overline{dK_{vv}}}{d\Omega}}$$
(2)

<sup>195</sup> It should be pointed out that laser energy attenuation and signal trapping at <sup>196</sup> 532 nm in the ethylene flame studied in this work may not be negligible at flame heights where soot volume fractions are fairly high. Nevertheless, such effects are neglected in the first attempt to demonstrate the capabilities of the HPALS technique and will be evaluated and taken into account in future studies.

Thus, for each scattering angle imposed by the angular position of the camera, the radially-resolved scattering coefficient can be retrieved by a simple inverse Abel transform  $(Ab^{-1})$  of the convoluted scattering signal profile acquired over the entire range of x,

$$\overline{\frac{dK_{vv}}{d\Omega}} = Ab^{-1} \left(\frac{P_{vv}}{I_0 \Omega dS}\right).$$
(3)

In order to determine the absolute value of the averaged scattering coefficient, a calibration of the detection system is necessary. In this study the calibration is performed by measuring the scattered signal produced by a free jet of ethylene  $P_{vv,C_2H_4}$ . At ambient conditions, the molecule density and the corresponding scattering cross section [22] are known. The resultant scattering coefficient is found to be  $K_{vv,C_2H_4} = 8.92 \times 10^{-6} m^{-1}$ .

It is noticed that the collected scattering signals from the flame soot as well as from the ethylene jet are systematically normalized by the corresponding laser intensity, number of accumulated images and camera gain, the absolute scattering coefficient of soot is then given by:

$$\frac{\overline{dK_{vv,soot}}}{d\Omega} = K_{vv,C_2H_4} \times \frac{Ab^{-1}\left(P_{vv,soot}\right)}{Ab^{-1}\left(P_{vv,C_2H_4}\right)}.$$
(4)

The measured profile  $(P_{vv,C_2H_4})$  and its deconvolution  $Ab^{-1}(P_{vv,C_2H_4})$  are given in Appendix A.

#### 217 3.2. Interpretation of scattering coefficient based on the RDGFA theory

For an ensemble of monodisperse aggregates and under conditions where the RDGFA theory is considered valid [22], the aggregate differential scattering coefficient can be expressed as,

$$\frac{dK_{vv,soot}}{d\Omega} = N_{agg} \frac{9\pi^2}{\lambda^4} F(m) V_{agg}^2 f(qR_g, D_f).$$
(5)

where  $N_{agg}$  and  $V_{agg}$  are respectively the aggregate number density and the individual aggregate volume, *m* is the soot complex refractive index, F(m) =  $|\frac{m^2-1}{m^2+2}|$  is the scattering function of m,  $\lambda$  is the incident laser wavelength, fis the structure factor,  $R_g$  is the gyration radius (the radius of an equivalent sphere having the same inertia moment), and  $q = \frac{4\pi}{\lambda} \sin\left(\frac{\theta}{2}\right)$  is the magnitude of scattering wave vector. Symbol  $D_f$  is the aggregate fractal dimension. The scaling law correlating the aggregate volume to its gyration radius is expressed as

$$N_p = \frac{V_{agg}}{V_p} = k_f \left(\frac{D_g}{D_p}\right)^{D_f},\tag{6}$$

where  $N_p$  is the number of primary spheres,  $V_p$  is the volume of primary sphere,  $D_g = 2R_g$  is the aggregate gyration diameter,  $D_p$  is the diameter of the primary spheres,  $k_f$  is the fractal prefactor (assumed equal to 2.2 in the present study, consistent with TEM measurements, e.g. [46]). We will also assume a typical value of  $D_f = 1.77$  for flame-generated soot, which is also the value of aggregates generated by diffusion-limited cluster aggregation (DLCA).

The structure factor formulated by Dobbins and Megaridis [47] is used in the present study because it has been shown to be accurate for the determination of the aggregate gyration radius based on light scattering at 532 nm even when considering the aggregate internal multiple scattering [40].

For polydisperse aggregates, by introducing the soot volume fraction as  $f_v = N_{agg} \times \overline{V_{agg}}$  and by using the factal scaling law (Eq. 6), the population averaged scattering coefficient can be expressed as,

$$\frac{\overline{dK_{vv,soot}}}{d\Omega} = \underbrace{\frac{9\pi^2}{\lambda^4} F(m) f_v \frac{\overline{V_{agg}^2}}{\overline{V_{agg}}}}_{Amplitude} \underbrace{\frac{R_g^{2D_f} f(qR_g, D_f)}{\overline{R_g^{2D_f}}}_{Size \ dependent}.$$
(7)

In this expression, we can distinguish the amplitude of the signal, which corresponds to the magnitude of the forward scattering signal ( $\theta = 0$ ), and the ratio  $\frac{\overline{R_g^{2D_f} f(qR_g,D_f)}}{\overline{R_g^{2D_f}}}$  that contains the angular dependence through the qparameter. In this study, the angular dependence term is interpreted in terms of aggregates size distribution. Moreover, the scattering amplitude is coupled with LOSA measurements (see [10]) and interpreted in order to determine the aggregates volume, density and primary sphere diameter.

#### 250 3.3. Soot aggregate size distributions

Interpretation of Eq. 7 requires some *a prior* knowledge of the size distribution density probability function. In the present study, three assumed distributions are considered, namely Monodisperse, Lognormal and Self-Preserving.

Due to the large particle number density and fairly high temperatures 255 in flames, it is highly unlikely that the aggregate sizes are monodisperse. 256 Nevertheless, this case is considered in order to test the sensitivity of the 257 methodology proposed to the assumed shape of aggregate size distribution 258 and to the magnitude of polydispersity. The Lognormal size distribution of 259 soot aggregates is considered because it is usually observed when expressed in 260 mobility diameter. Nevertheless, there is no theoretical basis to this empirical 261 observation in particular when the aggregate size is expressed by gyration 262 diameter. On the contrary, aggregation mechanisms for fractal aggregates 263 suggest a self-preserving size distribution [48]. Sorensen [22] pointed out that 264 this distribution can shorter the tail of the distribution for larger aggregates 265 compared to the Lognormal distribution, which is suspected to overestimate 266 the moments used for the evaluation of  $\overline{V_{agg}}$ ,  $\overline{V_{agg}^2}$ ,  $\overline{R_g^{2D_f}}f$  and  $\overline{R_g^{2D_f}}$  in Eq. 7. The lognormal distribution is governed by the geometric diameter  $D_{geo}$ 267 268 and the geometric standard deviation  $\sigma_{qeo}$ . The former is not so different from 269 the modal diameter of the distribution (most probable size). Caumont-Prim 270 et al. [30] reported  $\sigma_{geo} = 1.7$  based on angular light scattering measurement 271 in an ethylene flame for mature soot. The same author found 1.6 when 272 applying the technique on soot at the exhaust of a miniCAST generator. 273 The latter value (1.6) will be considered here since the exhaust of miniCAST 274 provides a uniform soot source avoiding issues related to the spatial resolution 275 of the conventional light scattering technique. This is also in agreement with 276 the values reported by Bouvier et al. [32]. However, it is noticed that some 277 authors considered larger values of the geometric standard deviation [29, 48]. 278 The self-preserving distribution is governed by a  $D_g$  and by the self-279 preserving homogeneity coefficient  $\lambda_{SP}$ . The latter parameter controls the 280 shape of the distribution. It has been reported to vary over a range of phys-281 ical values between -0.5 and 0.5 depending on the aggregation mechanisms, 282 which are principally driven by the primary sphere diameter (positive when 283 ballistic and negative when diffusive). In the present study, we hypothesize 284

that this parameter takes the value of null ( $\lambda_{SP} = 0$ ) as a result of aggregation occurring in the transition regime with a typical primary particle diameter <sup>287</sup> about 20 nm (see [48]). The size driving parameter  $\widetilde{D_g}$  is related to a moment <sup>288</sup> of the size distribution at power  $D_f$ , indeed  $\widetilde{D_g} = \left(\overline{D_g^{D_f}}\right)^{1/D_f}$  [48]. In con-<sup>289</sup> sequence, this parameter becomes larger as the aggregates are increasingly <sup>290</sup> more polydisperse.

A theoretical analysis of the self-preserving distribution, which has been shown to be a generalized gamma function [48], has shown that  $D_{g,modal} =$  $\widetilde{D_g} \left(1 - \frac{1}{D_f(1-\lambda_{SP})}\right)^{1/D_f}$  with  $D_{g,modal}$  being the mode of the distribution. In the present case where  $D_f$  and  $\lambda_{SP}$  are fixed respectively at 1.77 and 0, one can find  $\widetilde{D_g} = 1.57 \times D_{g,modal}$ . Thus, it is important to keep in mind that  $\widetilde{D_g}$  is consistently larger than the most probable gyration diameter (mode of the distribution).

The analytical expressions for  $\overline{R_g^{2D_f}f}$  and  $\overline{R_g^{2D_f}}$  under the hypothesis of Monodisperse, Lognormal and Self-Preserving distributions are presented in Appendix B.

#### 301 4. Results and Discussion

#### 302 4.1. Results at HAB = 30 mm

Figure 4 presents in black dots the radially-resolved scattering signals ex-303 pressed in  $K_{vv}$  measured at 22.4°, 33.9°, 51.1°, 80.2°, 90°, 119.8° and 148.1°, 304 for HAB = 30 mm through Abel inversion. The scattering wave vector q is 305 preferred over the direct use of scattering angle for the representation of an-306 gular dependence of scattering because this parameter is used in the RDGFA 307 theory. The scattered intensity decreases with increasing q, in particular for 308 large aggregates. Thus, at a given radial position r, the aggregate size dis-309 tribution can be obtained by fitting the curve in the q direction (e.g. the red 310 arrow in the graph). It should be pointed out that the aggregate size distri-311 bution determined does not depend on the amplitude of  $K_{vv}$  (green arrow in 312 graph). This point will be explained after. 313

The results of the aggregate size distribution parameters are reported in Fig. 5. In this figure, the points of red-circle are the gyration diameters of Monodisperse size distribution  $(D_g)$ , while the points of green-star and bluesquare are respectively the  $\widetilde{D_g}$  and  $D_{geo}$  for the self-preserving and lognormal distributions.

It is interesting to see that  $\widetilde{D}_g$  at power  $D_f$  corresponds to the population average gyration diameter at power  $D_f$  ( $\widetilde{D}_g^{D_f} = \overline{D}_g^{D_f}$ ). Due to the



Figure 4: Radial and angular distribution of the scattered signal at HAB = 30 mm after Abel inversion and expressed in terms of  $K_{vv}$ . The angular dependence of scattering is expressed through  $q = \frac{4\pi}{\lambda} \sin\left(\frac{\theta}{2}\right)$ , which is the magnitude of the scattering wave vector. The measured scattering signal is presented in black dots after the fitting process generating a continuous surface.

polydispersity, those parameters are lower than the equivalent gyration diameter under the assumption of monodisperse aggregates. Nevertheless, the assumption of monodisperse soot aggregates is clearly unrealistic in flames.

Therefore, we consider the lognormal or self-preserving hypothesis more representative of soot aggregates.  $\widetilde{D}_g$  is found to be somewhat larger than  $D_{geo}$  even though the self-preserving size distribution is lower than the lognormal one for small aggregates (see the inset of Fig. 5). This behavior is attributed to the definition of  $\widetilde{D}_g$  which represents a moment of power  $D_f$ , whereas  $D_{geo}$  is the median diameter.

It is interesting to notice that larger aggregates are found at a radial position between r = 2.9 and 3.0 mm whereas the signal amplitude starts to decrease at this radial distance at HAB = 30 mm (see Fig. 4).

The band that bounds each curve by dotted lines in Fig. 5 indicates the fitting quality. The band height is evaluated by considering the variance of



Figure 5: Radial profiles of soot gyration diameter distribution parameters at HAB=30 mm. The three profiles correspond to monodisperse, logNormal ( $\sigma_{geo} = 1.6$ ), and self-preserving ( $\lambda_{SP} = 0$ ) density probability functions. The bands between the dotted lines around each curve are an indication of the reliability level of the results. The inset illustrates the three aggregate size distributions at r = 3.1 mm.

experimental measurements around the fitted model. It should be noticed, 335 however, that the band height is not the measurement uncertainty since it is 336 very difficult to evaluate the latter. Nevertheless, we can consider the band 337 height as a proxy to the measurement uncertainty. In consequence, we can 338 see the uncertainty relative to the soot aggregate size is larger on the outer 339 edge of the flame wing. This is in part caused by the lower signal intensity 340 in this region. For  $r \leq 2.8$  mm, the fitting quality is slightly better for 341 the Lognormal and the Self-Preserving distributions than the Monodisperse 342 one. For the two polydisperse distributions (LN and SP) the fitting quality is 343 essentially the same over the entire radial range at HAB = 30 mm, suggesting 344 that it is impossible to say which distribution is a better representation of 345 soot aggregate size based on the fitting quality alone. 346

In addition to the determination of aggregate size distribution parameter, the fitting process of the recorded signals (Fig. 4) also enables an extrapolation of the forward scattering intensity  $(K_{vv}(0^o))$  corresponding to the amplitude term in Eq. 7. The results are reported in Fig. 6-A for the three assumed aggregate size distributions.  $K_{vv}(0^o)$  is clearly affected by the hypothesis of the aggregate size distribution primarily in the amplitude but also slightly in the radial position of the peak.

The forward scattering intensity is determined by the soot volume fraction 354  $f_v$ , scattering function of the refractive index F(m), and ratio of aggregate 355 volume moments  $\overline{V_{agg}^2}/\overline{V_{agg}}$ . In order to extract the moment ratio, we di-356 vide the amplitude term by  $f_v$  and F(m), which are reported in Fig. 6-B 357 at HAB = 30 mm. The volume fraction  $f_v$  has been determined by LOSA 358 measurements at multiple wavelengths (500, 532, 660 and 810 nm) in order 359 to take into account the influence of maturity dependence of soot optical 360 properties [10]. The value of F(m) is derived from the spectral dependence 361 of absorption function E(m), which in turn provides the soot maturity in-362 dex and finally the absolute absorption function E(m) (see [10]). The same 363 methodology can be used to infer the scattering function F(m) in the present 364 study (see Appendix C by utilizing the relationship between maturity in-365 dex and F(m)). Nevertheless, it should be pointed out that according to 366 the model used the change of scattering function at 532 nm is fairly weak 367 compared to the change of absorption function (see [10]). Thus, the impact 368 of soot maturity on the scattering function is less pronounced. 369

Figs. 6-B and 6-A clearly show a shift among the maximum volume frac-370 tion (at  $r \approx 2.6$  mm), scattered intensity ( $r \approx 2.8$  mm) and sharp increase 371 of maturity ( $r \approx 2.95$  mm). The corresponding ratio  $\overline{V_{aqq}^2}/\overline{V_{agg}}$  for the three 372 assumed distributions is reported in Fig. 6-C. This ratio remains almost the 373 same as the average aggregate volume for  $r \leq 2.3 mm$ ; however, it shifts 374 slightly towards larger values at larger radial positions for polydisperse ag-375 gregate distributions. In addition, the ratios for the lognormal distribution 376 are seen to be slightly larger than those of the self-preserving distribution. 377

The increase in  $\overline{V_{agg}^2}/\overline{V_{agg}}$  with increasing r suggests an increase in the average aggregate volume and in the aggregate polydispersity up to the outer edge of the flame. The even higher values of this ratio beyond r = 3.25 mm, where soot volume fraction drops to zero, are unphysical and can be considered a result of noise.

On the other hand, it can be seen from Fig. 6-C that the uncertainty in  $\overline{V_{agg}^2}/\overline{V_{agg}}$ , which is based on the propagation of error of the amplitude and



Figure 6: Radial profiles of selected properties of soot particles at HAB = 30 mm. A) Amplitude of the signal extrapolated at forward scattering  $K_{vv}(0)$ . B) Radial distribution of soot volume fraction  $f_v$  and scattering function F(m) according to [10]. C) Ratio of aggregates volumes momentum's  $\overline{V_{agg}^2}/\overline{V_{agg}}$ . The three profiles in the top and bottom plots correspond to data interpretation for the assumed three aggregate gyration diameter distributions: monodisperse, lognormal ( $\sigma_{geo} = 1.6$ ), and self-preserving ( $\lambda_{SP} = 0$ ).

volume fraction terms, also increases with increasing r due to the decrease 385 of  $f_v$ . Up to  $r \approx 2.9$  mm, it is not surprising to observe an increase of the 386 aggregate volume since the aggregate size increases (see Fig. 5). However, it 387 is less obvious for the increase in the ratio at larger r where the aggregate 388 size decreases, Fig. 5. This may be interpreted by an increase of the primary 389 sphere radius. Indeed, as shown in Table 1, the representative aggregate 390 volume term (the ratio of aggregate volume moments) depends on not only 391 the aggregate gyration diameter but also the primary sphere diameter  $D_p$ . 392 At this point, the aggregate size distribution is already determined thus the 393 radial behaviour of the primary sphere diameter can be established (see Fig 7-394 A). Because this quantity depends not only on the amplitude and angular 395 variation of the scattered signal but also on the soot volume fraction and the 396 morphological parameters  $(D_f \text{ and } k_f)$ , its uncertainty is relatively large. For 397 example, a lower fractal prefactor will cause an increase in the determined 398 primary sphere diameter. Again, the band bounded by two dotted lines 399 around each curve indicates the uncertainty based on error analysis. These 400 curves clearly show large uncertainties in the inner and outer regions of the 401 flame along the radial direction. 402

It is noticed that the obtained primary sphere diameters are in reasonably 403 good agreement with results reported in the literature. At the same HAB, 404 Botero et al. [49] found by TEM image analysis in a laminar coflow diffusion 405 flame over the Yale burner and fueled with nitrogen diluted ethylene that 406 the primary soot particles have a modal diameter of 21 nm with a high 407 polydispersity. Slightly larger values have been reported by Kempema and 408 Long [35]. In the same burner as in the present study and also for pure 409 ethylene, Cortés et al. [46] also performed TEM image analysis and found at 410 a similar location (HAB = 27 mm) and oxygen index (21%) that the primary 411 soot particles have a geometric mean diameter of 16 nm and a geometric 412 standard deviation of 1.6. Considering that Rayleigh scattering is a process 413 proportional to  $D_p^6$ , the results of Cortés et al. [46] can be reanalysed in terms 414 of the optical equivalent primary sphere diameter by using the Hatch-Choate 415 equation (average primary diameter at power 6) to yield 31 nm, in very close 416 agreement with the present results. Indeed, we observe  $D_p \approx 32$  nm in the 417 region where the uncertainties are low (see Fig 7-A)). 418

The region of low uncertainties  $(2.6 \le r \le 2.85)$  displays a locally increasing trend of the primary sphere diameter with increasing r that can be related to the surface growth process. This region also corresponds to the rapid increase in soot maturity as shown by the red dashed curve in Fig 6-B.



Table 1: Analytical expressions for the ratio of aggregate volume moments for monodipserse, lognormal, and self-preserving size distributions.

Figure 7: Radial profiles of some soot properties inferred from light scattering measurements at HAB = 30 mm. A) Primary sphere diameters  $D_p$ , B) Number of primary spheres per aggregate  $N_p$  related to the representative diameter and C) Aggregates number density  $N_{agg}$ . The three curves correspond to results for Monodisperse, Lognormal ( $\sigma_{geo} = 1.6$ ) and Self-Preserving ( $\lambda_{SP} = 0$ ) density probability function hypotheses.

In addition, since gyration diameter and primary sphere diameter are determined, we can evaluate the corresponding representative number of primary spheres  $(N_p)$  per aggregate employing the fractal law (Eq. 6). The result is reported in Fig 7-B. As already discussed for the gyration diameter,  $N_p$  is found to be larger if the aggregates are assume to be monodisperse.

The maximum average number of primary spheres per aggregate (at about 428 r = 2.74 mm is found slightly shifted toward the flame centerline compared 429 to the maximum representative gyration diameter (at about r = 3.0 mm, 430 Fig 5). This is explained by the increase of the primary sphere diameter due 431 to the surface growth. Assuming lognormal and self-preserving aggregate 432 gyration diameter distributions, the determined maximum average number 433 of primary spheres per aggregate is found to be 46 and 58 at HAB = 30 mm, 434 respectively. 435

Finally, the aggregate number density can be determined. Indeed, it is evaluated as  $N_{agg} = f_v / \overline{V_{agg}}$ , with  $\overline{V_{agg}} = \pi D_p^{3-D_f} k_f \overline{D_g^{D_f}} / 6$  and  $\overline{D_g^{D_f}}$  is given in Appendix B according to the type of assumed aggregate size distribution. The results are reported in Fig 7-C. The aggregate number density decreases with increasing r due to aggregation. At radial positions larger than about r = 2.75 mm, we observe a decreasing aggregate number density (Fig 7-C) of smaller aggregates (Fig 7-B), which seems composed of large primary spheres (Fig 7-A).

#### 444 4.2. Results at different HAB

The methodology described above has also been applied to different heights 445 above the burner. To highlight the capability of the proposed light scat-446 tering technique and focus on the measured soot properties in the laminar 447 diffusion flame, we only report below the results based on the hypothesis of 448 self-preserving aggregate size distribution, which is supported by theoretical 449 considerations as mentioned in Section 3.3. It is also useful to recall that 450 the corresponding governing parameter  $\widetilde{D}_g$  is larger than the modal diam-451 eter of the distribution by a factor 1.57, which results from its moment at 452 a power  $D_f$  (see discussion in Section 3.3). Therefore, the corresponding 453 average number of primary spheres per aggregate will be also slightly larger 454 as seen in Fig 7-B. 455

Figures 8 and 9 report respectively the radial profiles of the self-preserving governing parameter  $\widetilde{D}_g$  and the corresponding average number of primary spheres per aggregate  $N_p$  at different HAB. The corresponding uncertainties

are represented by the error bars. Clearly, an intense particle aggregation 459 takes place along the flame wing region up to about HAB = 45 mm, followed 460 by a significant decrease of aggregate size at higher HAB. Indeed, simulations 461 performed with the CoFlame code [50] (reported in Appendix D) indicate 462 that particle nucleation, coagulation, and surface growth via surface reactions 463 (HACA) and PAH adsorption processes govern soot production at the lower 464 part of the flame, leading to increased number and diameter of primary 465 particles. These particles are convected downstream where the oxidation 466 processes by OH radicals and O<sub>2</sub> molecules are dominant, causing a decrease 467 in their size and eventually complete oxidation. 468

To our knowledge, there have been no studies of *in situ* determination 469 of the aggregates size in the flame wing region of a pure ethylene diffusion 470 flame established over the Gülder burner. Therefore, it is challenging to di-471 rectly compare our present results with those of previous studies. Kempema 472 and Long [35] applied 2D-MALS (multi-angle light scattering) in a nitrogen 473 diluted ethylene flame  $(20\%C_2H_4 \text{ and } 80\%N_2)$  over the Yale coflow burner 474 and found similar profiles. The monodisperse equivalent gyration diameters 475 they reported was about 440 nm, which is much smaller that the maximum 476 values reported in the present work. However, it should be noted that for 477 larger aggregates  $(D_q \ge 200 \ nm)$ , the fractal dimension can affect the size 478 measurement since part of the collected signal emanates from the power-law 479 regime. Thus, the uncertainty associated with the largest diameters, and 480 thus in particular for HAB = 45 mm, can become significant. Moreover, 481 the different fuels and burners between our work and previous studies may 482 largely explain the difference. Finally, we believe that the present technique 483 offers a greater spatial resolution, enabling to properly resolve the aggregate 484 sizes in the flame region of high gradients. Indeed, we show in Appendix E 485 that the classical 2D-MALS can underestimate the peak gyration diameter 486 detected at HAB = 40 mm by about 100 nm due to the change of mea-487 surement volume with the scattering angle. Nevertheless, this strong effect 488 seems to appear only in the presence of large spatial gradients of aggregate 489 size distribution parameter. 490

The largest aggregates in terms of  $\widetilde{D}_g$  are found at HAB = 40 mm, whereas larger values of  $N_p$  seem to be at HAB = 55 mm. This difference may be explained by the smaller primary spheres at HAB = 55 mm (see Figure 10). Kempema and Long [35] reported median numbers of monomers per aggregate between 47 and 71 along the centerline, and between 14 to 16 along the wing of a flame established over the Yale coflow burner. Although the presently reported values are larger than those of Kempema and Long [35], it should be noticed that in addition to the different flame conditions the present results correspond to the number of primary sphere of the representative size parameter  $\widetilde{D}_g$ , which is not the median parameter reported by Kempema and Long [35].

Due to the large uncertainties related to the primary sphere diameter 502 determination, we only report in Figure 10 the representative values along 503 HAB. These values are the primary sphere diameter whose uncertainty is 504 the lowest in the radial profile at the given HAB. The overall decreasing 505 trend in the representative primary sphere diameter above HAB = 50 mm506 shown in this figure confirms the strong oxidation process in the upper part 507 of the flame, which is also qualitatively observed from the predictions of the 508 simulated flame (see Appendix D). The results are also in reasonably good 509 agreement with the TEM image analysis reported in [35]. 510



Figure 8: Radial profiles of the aggregate size distribution parameter in the self-preserving distribution assuming ( $\lambda_{SP} = 0$ ) at different HAB.



Figure 9: Radial profiles of the average number of primary spheres per aggregate at different HAB.

At low HAB, soot is present only in the flame wing region. With increas-511 ing HAB, soot starts to appear in the flame centreline region. At upper part 512 of the flame  $(55 \le HAB \le 70 \text{ mm})$ , the aggregate size seems relatively uni-513 form in the centerline region within about  $r \leq 1.5$  mm. Aggregation seems 514 less intense in this region compared to the outer flame edge. Nevertheless, at 515 the flame centerline large aggregates can be found at HAB = 60 mm (up to 516 about 200 nm) but then decrease to about 150 nm at HAB = 70 mm. This 517 decrease is mainly caused by the decrease of primary sphere diameters while 518 the number of primary spheres still increases. Because this region is marked 519 by a strong reduction of soot material (decrease of volume fraction shown in 520 Appendix C), we can speculate that the soot oxidation in this region of the 521 flame is likely a surface process which mainly reduces the diameter of the 522 primary spheres. Moreover, the aggregation process seems to compensate 523 the possible fragmentation process to some extent. 524



Figure 10: Variation of the representative primary sphere diameter along HAB. The representative primary sphere diameter at each HAB is the value whose uncertainty is the lowest.

Figure 11 presents the radial profiles of aggregate number density at different HAB. The vertical bars represent the uncertainty for each value of  $N_{agg}$ . The gradient of this parameter remains very large on the flame wings <sup>528</sup> up to about HAB = 50 mm, above which soot particles in the centerline <sup>529</sup> region can be detected.

Although some soot particles in the centerline region may be convected from the outer region, soot particles in this region are believed to be mainly composed of nucleation soot with smaller aggregates and immature (lower E(m) and F(m)). In this region, the number density is seen to be between  $3 \times 10^{10}$  and  $8 \times 10^{10}$  particles/ $cm^3$ , in good agreement with [23, 51] which reported  $N_{agg} \sim 10^{10}$  cm<sup>-3</sup> in similar ethylene diffusion flames.



Figure 11: Radial profiles of the aggregates number density at different HAB.

#### 536 5. Conclusion and perspectives

The present experimental investigation complements our recent study using a multiple-wavelength LOSA analysis for the determination of soot volume fraction and maturity in a laminar coflow ethylene/air diffusion flame produced using a Gülder burner. In the present work, the spatial distribution of aggregate size is determined by elastic angular light scattering. The originality of the proposed technique lies in optical setup using a laser sheet arranged horizontally through the flame and we named this method the Horizontal Planar Angular Light Scattering (HPALS). This setup avoids the issues related to a significant change of the measurement volume with the scattering angle making the conventional light scattering techniques challenging to apply to flames where soot properties display strong gradients.

The Horizontal Planar Angular Light Scattering technique introduced in this work enables a description of soot characteristics with an extremely high spatial resolution, though it is necessary to conduct Abel inversion.

The coupling of HPALS with LOSA enables a comprehensive description 551 of soot volume fraction, size (aggregate and primary sphere), and number 552 density. The limitation of this technique is that it can only be applied to 553 axisymmetric laminar flames. The coupling of HPALS and multi-wavelength 554 LOSA paves the way to provide a more complete description of soot proper-555 ties and hence helps improve our understanding of soot formation and oxida-556 tion mechanisms. The present work also enables a complete database of soot 557 properties that is useful for validation of soot models able to consider the 558 aggregation mechanisms. Additionally, the high spatial resolution of HPALS 559 allows to improve and validate the coagulation models in regions of steep 560 gradients where the conventional light scattering techniques cannot properly 561 resolve soot properties, such as  $N_{aqq}$  and  $N_p$ . In summary, the combination 562 of HPALS and multi-wavelength LOSA offers a powerful diagnostic tool to 563 provide improved description of soot properties related to aggregate size. 564

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#### 572 Appendix A. Calibration of the scattered signal

<sup>573</sup> Figure A.12 shows the radial profile of the acquired scattering signal be-

- <sup>574</sup> fore and after Abel deconvolution. The average level determined after de-<sup>575</sup> convoltion  $Ab^{-1}(P_{vv,C_2H_4}) = 0.0653$  is used to calibrate the scattering mea-
- surements.  $(T_{vv,C_2H_4}) = 0.00000$  is used to calibrate the scatter surements.



Figure A.12: The radial profiles of scattered signal obtained from a free jet of ethylene.

#### 577 Appendix B. Analytical expression of gyration radius related mo-578 ments

Equations B.1, B.2 and B.3 provide the analytical expressions of  $\overline{R_g^{2D_f}f}$ for monodisperse, lognormal, and self-preserving aggregate size distributions, respectively

$$\overline{R_g^{2D_f}f} = R_g^{2D_f}f(qR_g) \tag{B.1}$$

$$\overline{R_g^{2D_f}f} = \int_0^\infty \frac{D_g^{2D_f - 1} f(qR_g) e^{-\frac{1}{2} \left(\frac{\ln(D_g/D_{geo})}{\ln(\sigma_{geo})}\right)^2}}{2^{2D_f} \sqrt{2\pi} \ln(\sigma_{geo})} dD_g$$
(B.2)

$$\overline{R_g^{2D_f}f} = \int_0^\infty \frac{D_f}{2^{2D_f}} \frac{(1-\lambda_{SP})^{(1-\lambda_{SP})}}{\Gamma(1-\lambda_{SP})} \frac{D_g^{D_f(3-\lambda_{SP})-2}}{\widetilde{D_g}^{D_f(1-\lambda_{SP})}} f(qR_g) e^{-(1-\lambda_{SP}) \left(\frac{D_g}{\overline{D_g}}\right)^{D_f}} dD_g$$
(B.3)

Equations B.4, B.5 and B.6 are the analytical expressions of  $\overline{R_g^{2D_f}}$  for monodisperse, Lognormal, and self-preserving aggregate size distributions, respectively

$$\overline{R_g^{2D_f}} = R_g^{2D_f} \tag{B.4}$$

$$\overline{R_g^{2D_f}} = \left(\frac{D_{geo}}{2}\right)^{2D_f} e^{2D_f^2 ln^2(\sigma_{geo})} \tag{B.5}$$

$$\overline{R_g^{2D_f}} = \left(\frac{\widetilde{D_g}}{2}\right)^{2D_f} \frac{2 - \lambda_{SP}}{1 - \lambda_{SP}} \tag{B.6}$$

Equations B.7, B.8 and B.9 provide the analytical expressions of  $\overline{R_g^{D_f}}$  for monodisperse, lognormal, and self-preserving size distributions, respectively

$$\overline{R_g^{D_f}} = R_g^{D_f} \tag{B.7}$$

$$\overline{R_g^{D_f}} = \left(\frac{D_{geo}}{2}\right)^{D_f} e^{\frac{D_f^2 ln^2(\sigma_{geo})}{2}}$$
(B.8)

$$\overline{R_g^{D_f}} = \left(\frac{\widetilde{D_g}}{2}\right)^{D_f} \tag{B.9}$$

# Appendix C. F(m) and $f_v$ based on multi-wavelength LOSA measurements

Figure C.13 shows the radial profiles of soot volume fraction at different HABs. These profiles were computed by considering the dependence of the scattering function F(m) on the maturity coefficient  $\beta$ , as shown in Fig. C.14 (see [10] for details).



Figure C.13: Soot volume fraction as a function of the height above the burner (Data from [10])

#### <sup>593</sup> Appendix D. CoFlame simulation of the ethylene diffusion flame

To complement the experiments and to provide useful details of the 594 soot formation processes, the laminar coflow flame was simulated with the 595 CoFlame code [50]. Details of the simulation are provided in [10]. The 596 gas-phase kinetics is modeled with the DLR chemical mechanism [52]. The 597 transport equations for the flow, species, energy, and soot are solved in 598 a fully-coupled fashion. The population balance equations of soot aggre-599 gates and primary particles were solved using a sectional method consid-600 ering soot nucleation due to collision of three five-ring polycyclic aromatic 601 hydrocarbons (PAHs), surface growth via PAH adsorption (collision theory 602 and sticking probability) of the same PAHs onto soot surface and by the 603



Figure C.14: Relationship between the maturity coefficient and the scattering function using the same methodology described in [10].

hydrogen-abstraction carbon-addition (HACA) mechanism [53], which in-604 cludes surface oxidation by  $O_2$  (HACA) and OH (collision theory), particle 605 aggregation and oxidation-driven aggregate fragmentation. The rates of pro-606 duction/consumption by these processes are computed from the soot particle 607 characteristics and related species concentrations (see [50] for details). Fig-608 ure D.15 presents a qualitative description, from the converged solution of 609 the flame simulation, of the different regions of the flame where nucleation, 610 coagulation, PAH adsorption, HACA, OH and O<sub>2</sub> oxidation prevail. 611

#### <sup>612</sup> Appendix E. Superiority of HPALS over conventional approaches

The main advantage of HPALS over conventional scattering techniques, such as 2D-MALS, is its ability to provide high spatial resolution over a wide range of scattering angle (except very small scattering angles in the forward direction or very large scattering angles in the backward direction), i.e., the spatial resolution of HPALS is independent of the scattering angle.

Indeed, in classical configuration of light scattering experiments (vertical laser light sheet or horizontal laser beam crossing the flame centerline, see Fig.E.16), the volume of measurement, which corresponds to the intersection between the laser and the signal collection optics, increases when scattering angle deviates from  $\theta = \pi/2$ . When the scattering signal is detected by a CCD camera, the spatial resolution of measurement,  $\Delta r$ , is related to a pixel on the camera with a width  $\Delta x$ , through  $\Delta r = \Delta x/\sin(\theta)$ .



Figure D.15: Distributions of the different soot processes in the laminar ethylene diffusion flame based on the CoFlame simulation.

Therefore, even if the scattering intensity is corrected for the scatteringangle dependent measurement volume as in [34, 36], the detected scattering intensity is likely contributed from soot particles of different properties when the spatial resolution is poor at small and large scattering angles.

This tends to smooth the angle-resolved light scattering intensity, especially in the forward and backward directions. In consequence, the fitting process and the resulting radial distribution of aggregate size distribution parameters can be affected. This impact is evaluated in the present section. For this purpose, we consider the radial profile determined by HPALS since its spatial resolution is independent of scattering angle. To simulate the collected signals that would be measured by 2D-MALS after correction of



Figure E.16: Illustration of the change of measurement volume with changing the scattering angle in conventional vertical planar configuration (top view).

the intensity caused by angle-dependent measurement volume, the HPALS radial intensity profile is convoluted by a Gaussian function whose width is inversely proportional to  $sin(\theta)$ .

The convoluted signals are then processed using the same method as in 639 the present experiments. The results are compared at two HABs of 30 mm 640 and 40 mm, the later being the height where larger aggregates and stronger 641 gradients have been detected (see Fig.E.17). It is clear from this figure that 642 the reduced spatial resolution of 2D-MALS with varying scattering angle 643 leads to lower aggregate size distribution parameters in the radial region of 644 of strong gradients and of large aggregates around r = 2.6 mm at HAB = 645 40 mm. The effect is much less pronounced in regions where the gyration 646 diameter profile is relatively smooth at both HAB = 40 mm (outside the 647 peak region between about r = 2.5 mm and 2.7 mm) and 30 mm. It is also 648 interesting to notice that the simulated 2DMALS experiments artificially 649 enlarges the sooting region slightly at both HAB = 30 and 40 mm, which is 650 again caused by the reduced spatial resolution with varying scattering angles. 651



Figure E.17: Comparison of the gyration diameter governing parameter of the Self-Preserving size distribution obtained in the present study (HPALS) and as it should be measured with conventional vertical planar techniques as 2D-MALS. Comparison is performed at 2 HAB.

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